

①

Given:  $T_1 = 32^\circ\text{C}$ ;  $P = 101,3 \text{ kPa}$ ;  $\phi_1 = 80\% = 0,8$ ;

$T_2 = 10^\circ\text{C}$ ;  $\phi_2 = 40\% = 0,4$   $\dot{V} = 800 \frac{\text{m}^3}{\text{min}} = 13,33 \frac{\text{m}^3}{\text{s}}$

$R = 287 \frac{\text{J}}{\text{kg}\cdot\text{K}}$ ;  $C_p = 1005 \frac{\text{J}}{\text{kg}\cdot\text{K}}$

Part 1 (a) From saturated steam table we get

the saturated pressure at  $T_1$  using interpolation between  $30^\circ\text{C}$  and  $35^\circ\text{C}$

$$P_{s1} = 4,246 + \frac{(5,628 - 4,246)(32 - 30)}{35 - 30} = 4,799 \text{ kPa}$$

The vapor pressure at  $T_1$ :  $P_{v1} = P_{s1} \cdot \phi_1 = 4,799 \cdot 0,8 = 3,839 \text{ kPa}$

From saturated steam table we get the dew point temperature at  $P_{v1}$  using interpolation between 3 and 4 kPa

$$T_s = 24,08 + \frac{(28,96 - 24,08)(3,839 - 3)}{4 - 3} = 28,17^\circ\text{C}$$

(b) From saturated steam table we get vapor enthalpy at  $T_1$  using interpolation between  $30^\circ\text{C}$  and  $35^\circ\text{C}$

$$h_{v1} = 2556,3 + \frac{(2565,3 - 2556,3)(32 - 30)}{35 - 30} = 2560 \frac{\text{kJ}}{\text{kg}}$$

The enthalpies of vapor and liquid at  $T_2$  are:

$$h_{v2} = 2519,8 \frac{\text{kJ}}{\text{kg}}; \quad h_{e2} = 42,01 \frac{\text{kJ}}{\text{kg}}$$

Since vapor at  $T_2$  is saturated from steam table we get the vapor pressure at  $T_2$ :

$$P_{v2} = P_{\text{sat}} = 1,2276 \text{ kPa}$$

The specific humidity at  $T_1$  and  $T_2$ :

(2)

$$w_1 = 0,622 \frac{P_{v1}}{P - P_{v1}} = 0,622 \frac{3,839}{101,3 - 3,839} = 0,02450$$

$$w_2 = 0,622 \frac{P_{v2}}{P - P_{v2}} = 0,622 \frac{1,2276}{101,3 - 1,2276} = 0,007630$$

The heat removed at the cooling coil is:

$$q_{out} = C_p(T_1 - T_2) + w_1(h_{v1} - h_{e2}) - w_2(h_{v2} - h_{e2})$$

$$q_{out} = 1005(32 - 10) + 0,02450(2560 - 42,01) - 0,007630(2513,8 - 42,01)$$

$$q_{out} = 64,9 \frac{\text{kJ}}{\text{kg dry air}}$$

(c) The mass rate of dry air is given by

$$\dot{m}_g = \frac{(P - P_{v1}) \dot{V}}{RT_1} = \frac{(101,3 - 3,839) \cdot 13,33}{287(32 + 273,15)} = 14,84 \frac{\text{kg}}{\text{s}}$$

So the rate of condensate removal is

$$\dot{m}_e = \dot{m}_g w_1 - \dot{m}_g w_2 = \dot{m}_g (w_1 - w_2)$$

$$\dot{m}_e = 14,84(0,02450 - 0,007630) = 0,250 \frac{\text{kg}}{\text{s}}$$

(d) The specific humidity at the heating coil remains constant:  $w_3 = w_2$ .

From psychrometric chart we get the temperature at the exit of heating coil for  $w_3 = 0,00763$  and  $\phi_3 = 40\%$

$$T_3 = 24^\circ\text{C}$$

From steam table we get using interpolation between  $20^{\circ}\text{C}$  and  $25^{\circ}\text{C}$  for vapor

$$h_{v3} = 2532,1 + \frac{(2547,2 - 2532,1)(24 - 20)}{25 - 20} = 2545 \frac{\text{kJ}}{\text{kg}}$$

The heat rate added at the heating coil is:

$$\dot{q}_{in} = C_p(T_3 - T_2) + w_2(h_{v3} - h_{v2})$$

$$\dot{q}_{in} = 1005(24 - 10) + 0,007630(2545 - 2519,8) = 14,3 \frac{\text{kJ}}{\text{kg dry air}}$$

Part 2 I cannot do this part